

GRASSHOPPER

Grid Assisting Modular Hydrogen PEM Power Plant



# Modelling and optimization of a flexible PEMFC power plant for grid balancing purposes

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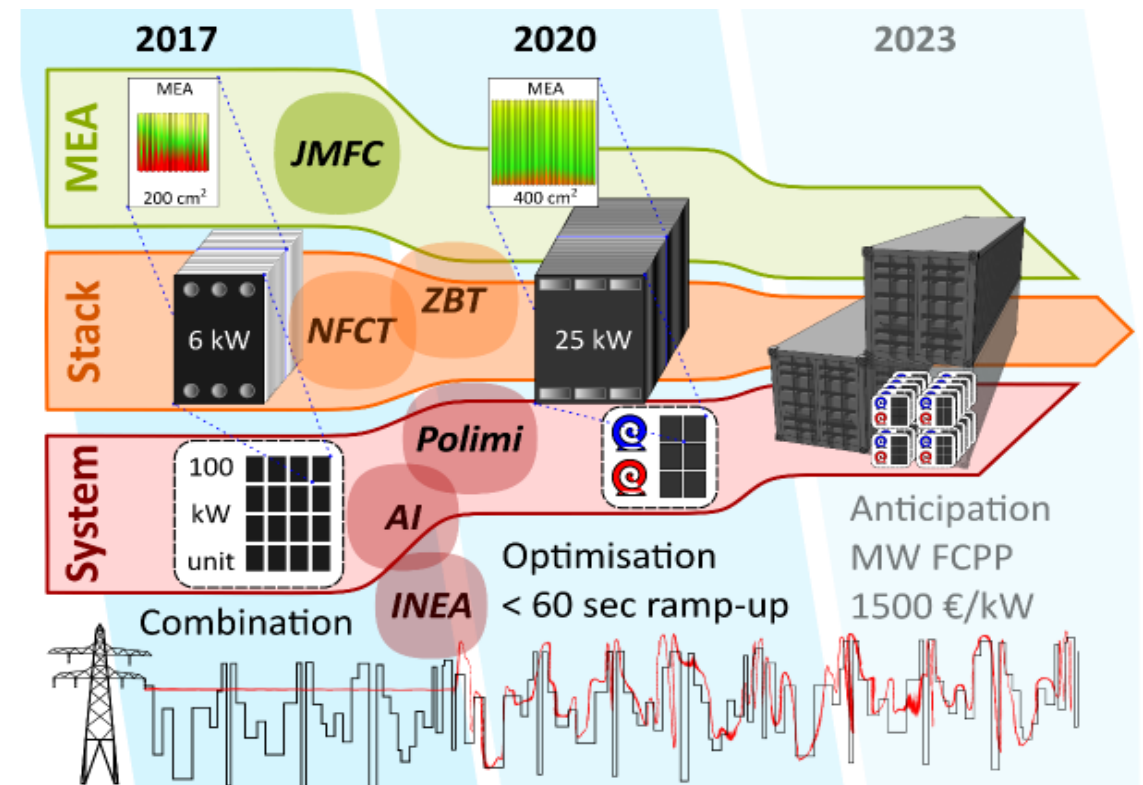


# GRASSHOPPER project



- ▶ This work is developed within the EU Project GRASSHOPPER, aiming at analysing how distributed and fast-ramping Fuel Cell Power Plants (FCPP) can be used to provide ancillary services and help balancing the grid.
- ▶ The project will setup and demonstrate a 100 kW<sub>el</sub> PEM FCPP unit:
  - ▶ cost-effective
  - ▶ flexible in power output
  - ▶ scalable to MW-size
  - ▶ for grid support with a Demand Side Management program

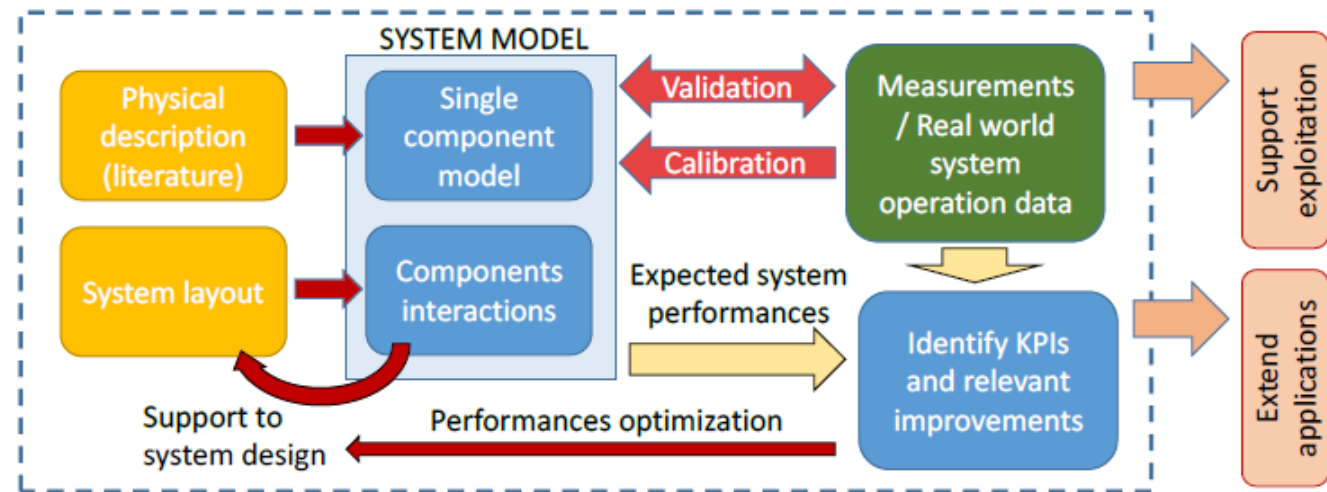
## Grid Assisting Modular Hydrogen PEM Power Plant



# Modelling activities



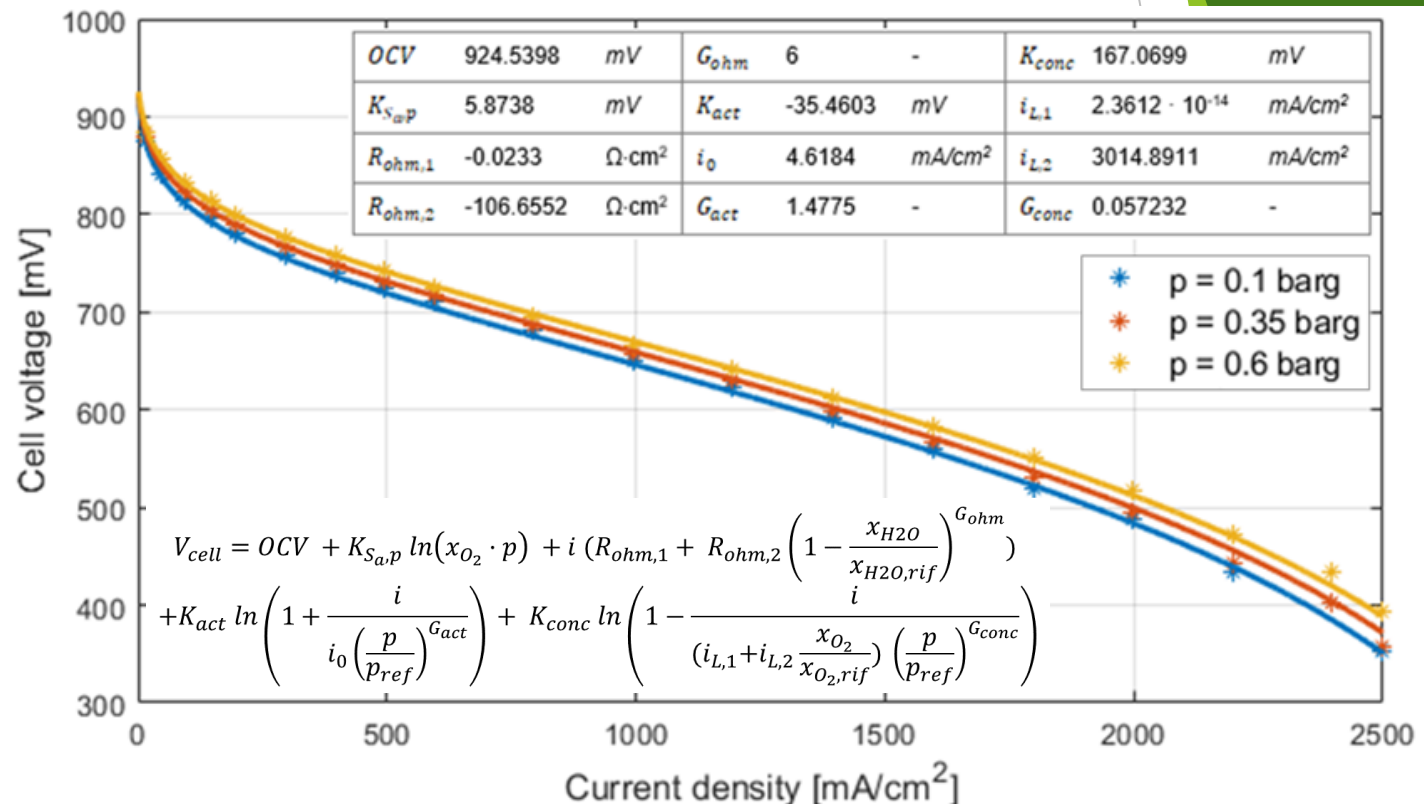
- ▶ Two different configurations for the GRASSHOPPER pilot plant are simulated to:
  - ▶ support the decisional process for defining the plant configuration;
  - ▶ optimizing the plant expected operating conditions and evaluate its performance;
  - ▶ to investigate the behaviour of the system in off-design conditions, influencing the definition of an optimized plant control strategy.
- ▶ A stationary model of the FCPP in Aspen Plus®:
  - ▶ PEMFC customized model
  - ▶ main balance of plant components



# Modelling approach: PEMFC model



- ▶ Lumped-volume approach.
- ▶ Semi-empirical equation of the cell polarization curve, including the effects of:
  - ▶ Stack backpressure
  - ▶ Air ratio to stoichiometry
  - ▶ Air relative humidity
- ▶ Regressions are made for a single cell:
  - ▶ relative errors always below 8%
  - ▶ Relative errors below 3% below 1.5 A/cm<sup>2</sup>

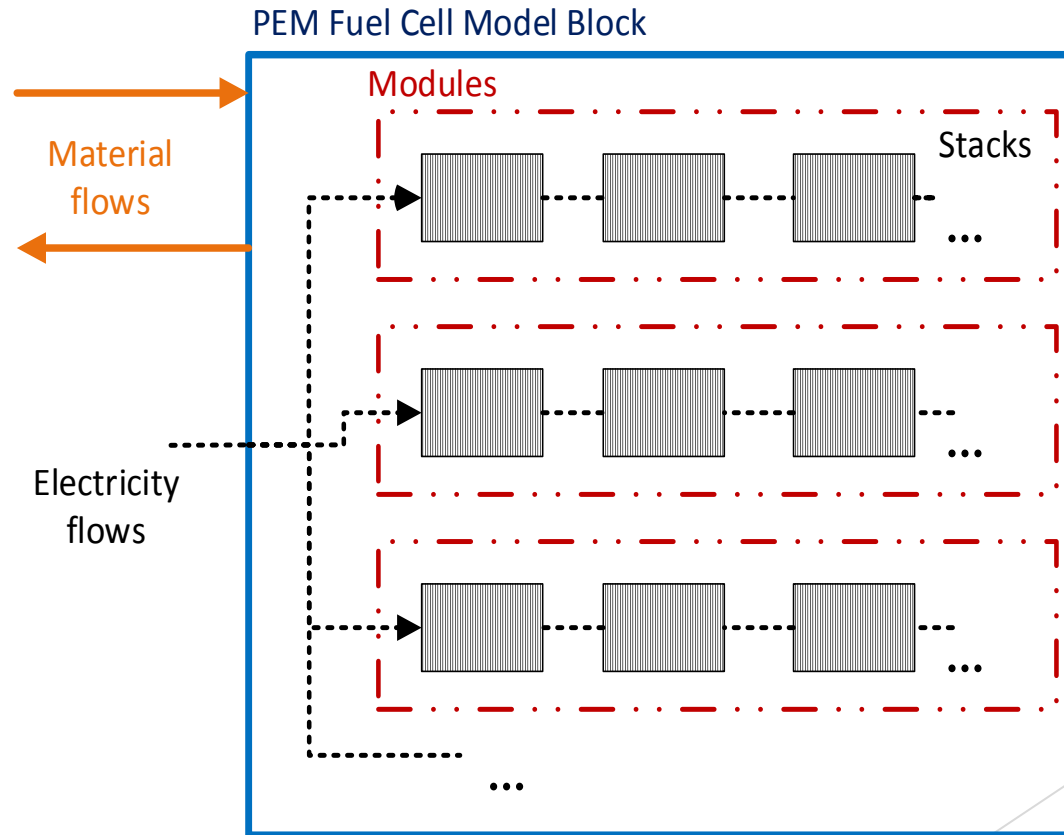


Cells polarisation curves obtained from CFD simulations at ZBT

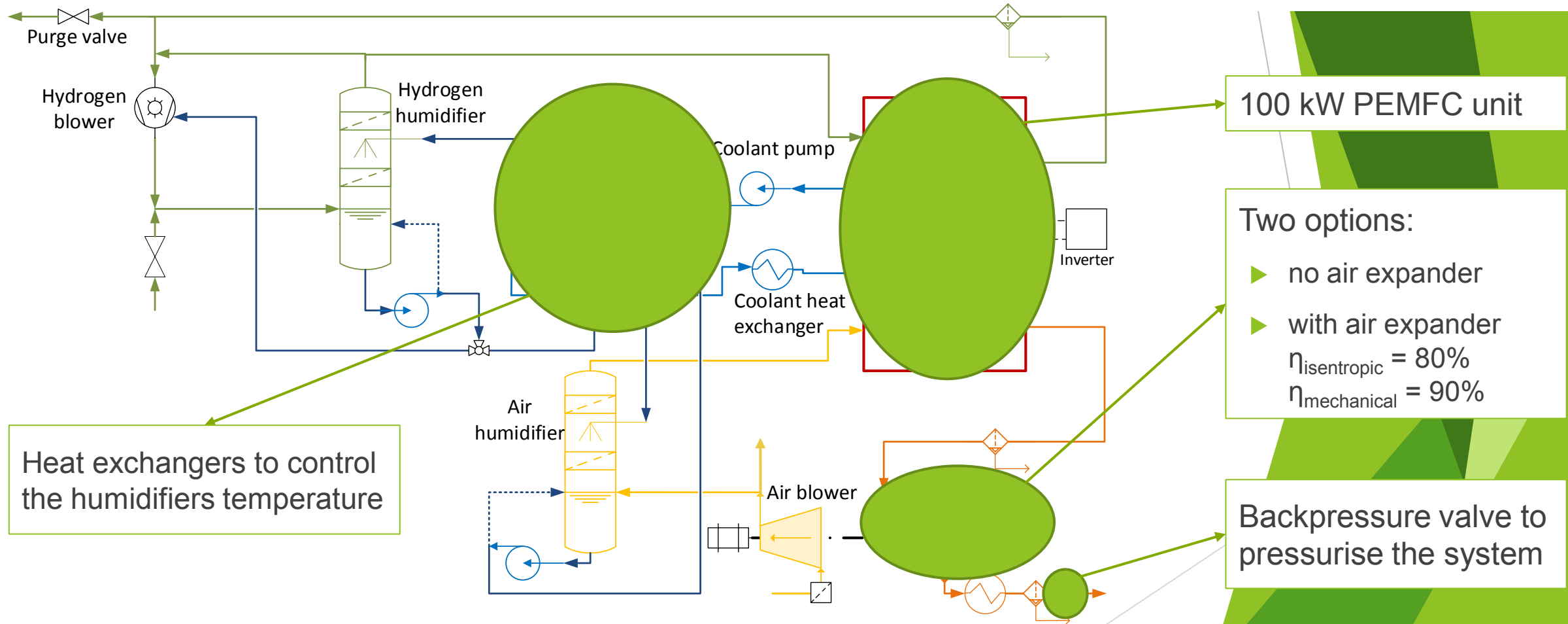
# Modelling approach: PEMFC model



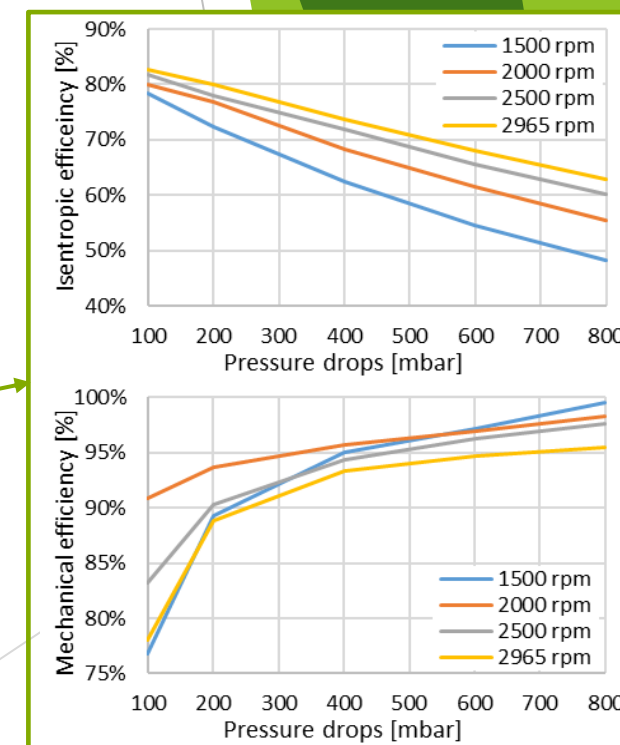
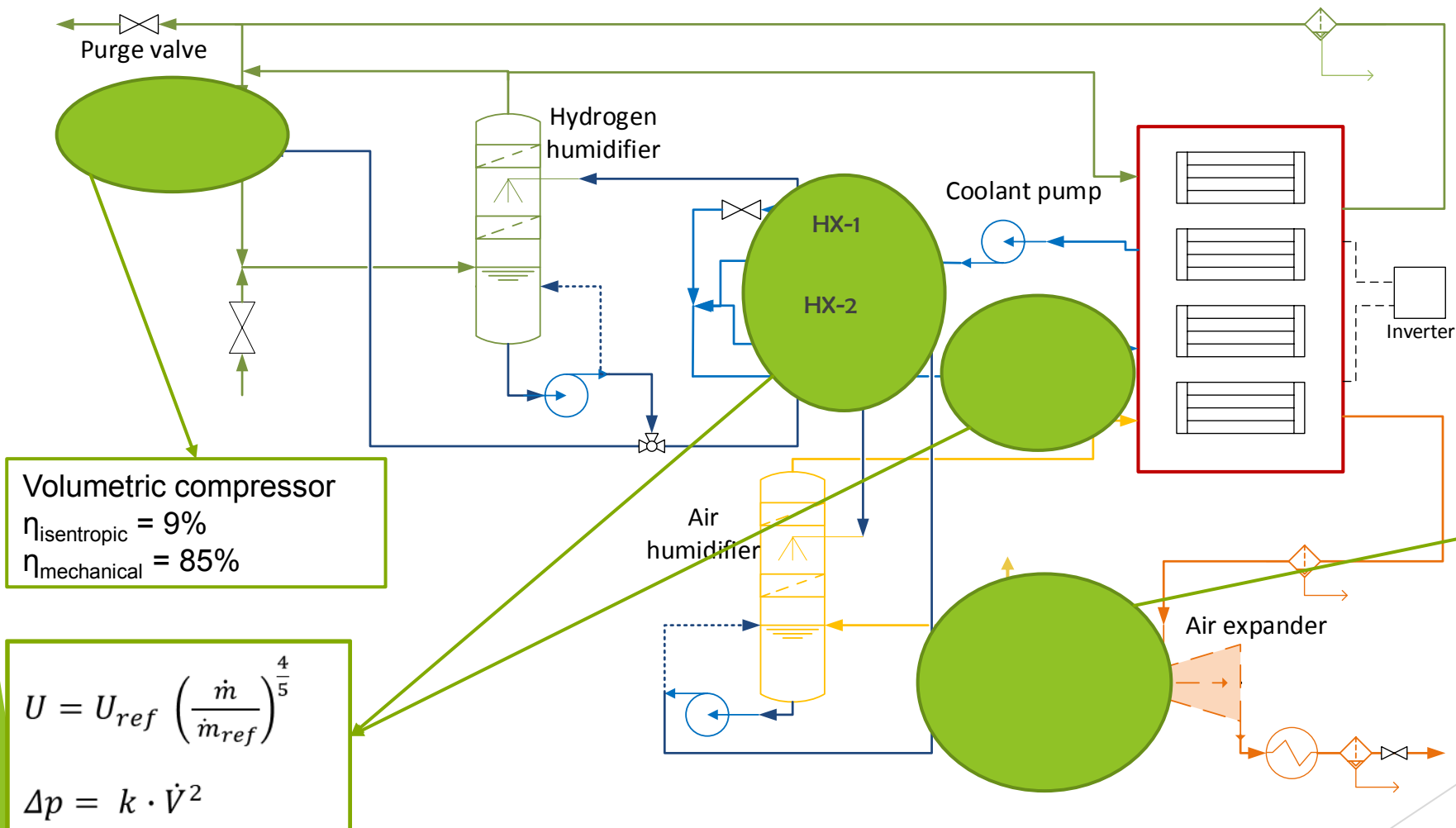
- ▶ Mass and energy balances are solved to determine cells outlet conditions.
- ▶ Pressure drops are a function of the flow rate.
- ▶ Cells model is modular: cells can be connected in series and in parallel to reach the desired power.



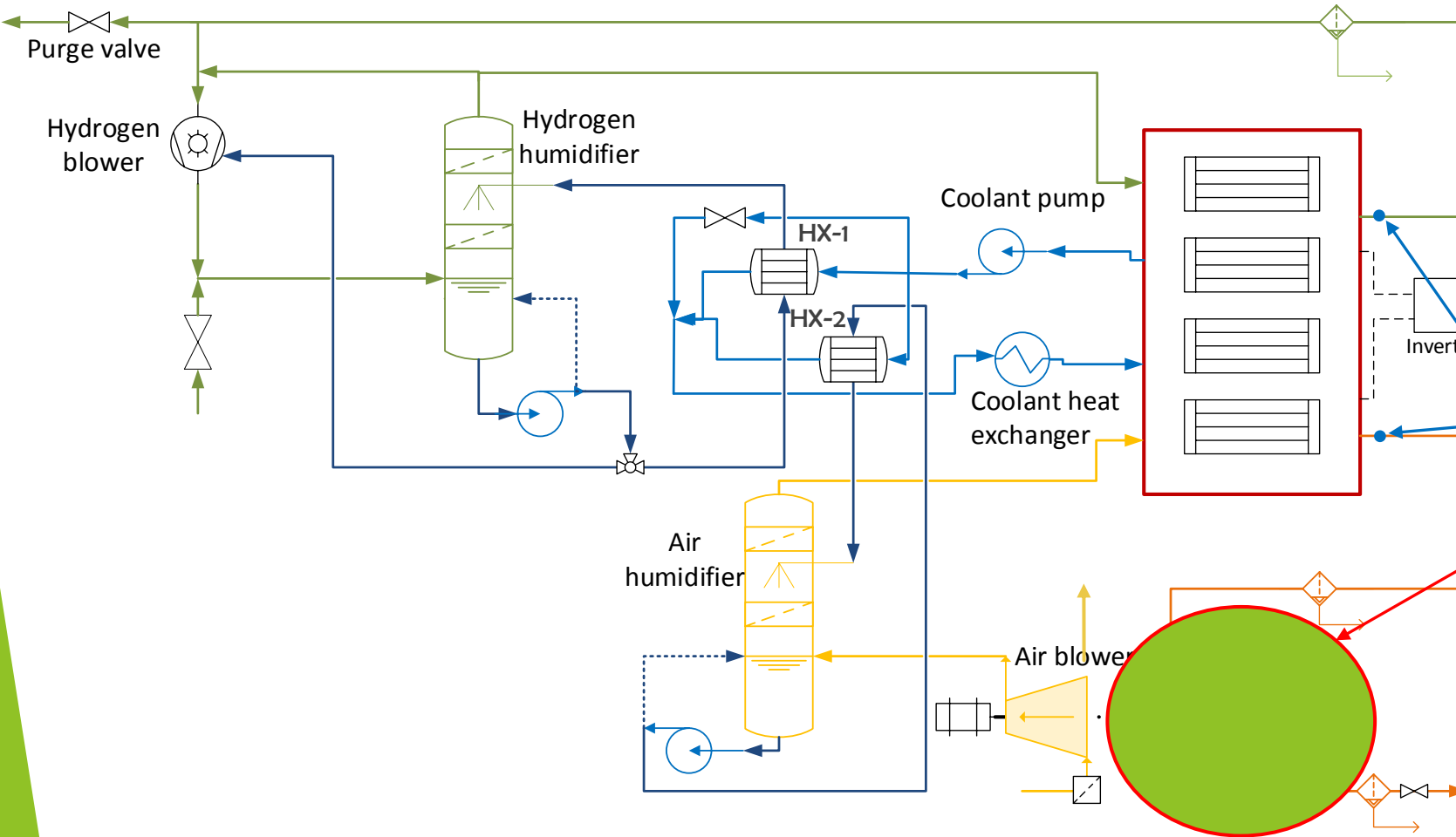
# Modelling approach: main BoP components



# Modelling approach: main BoP components



# Simulations



- ▶ Range of currents between 20% and 150% of the nominal current value ( $1 \text{ A/cm}^2$ ).
- ▶ Different stack **backpressure** and **plant configuration**:

Case 1	Case 2	Case 3	Case 4
Ambient pressure	Ambient pressure	Pressurised ( $0.6 \text{ bar}_g$ )	Pressurised ( $0.6 \text{ bar}_g$ )
No expander	With expander	No expander	With expander

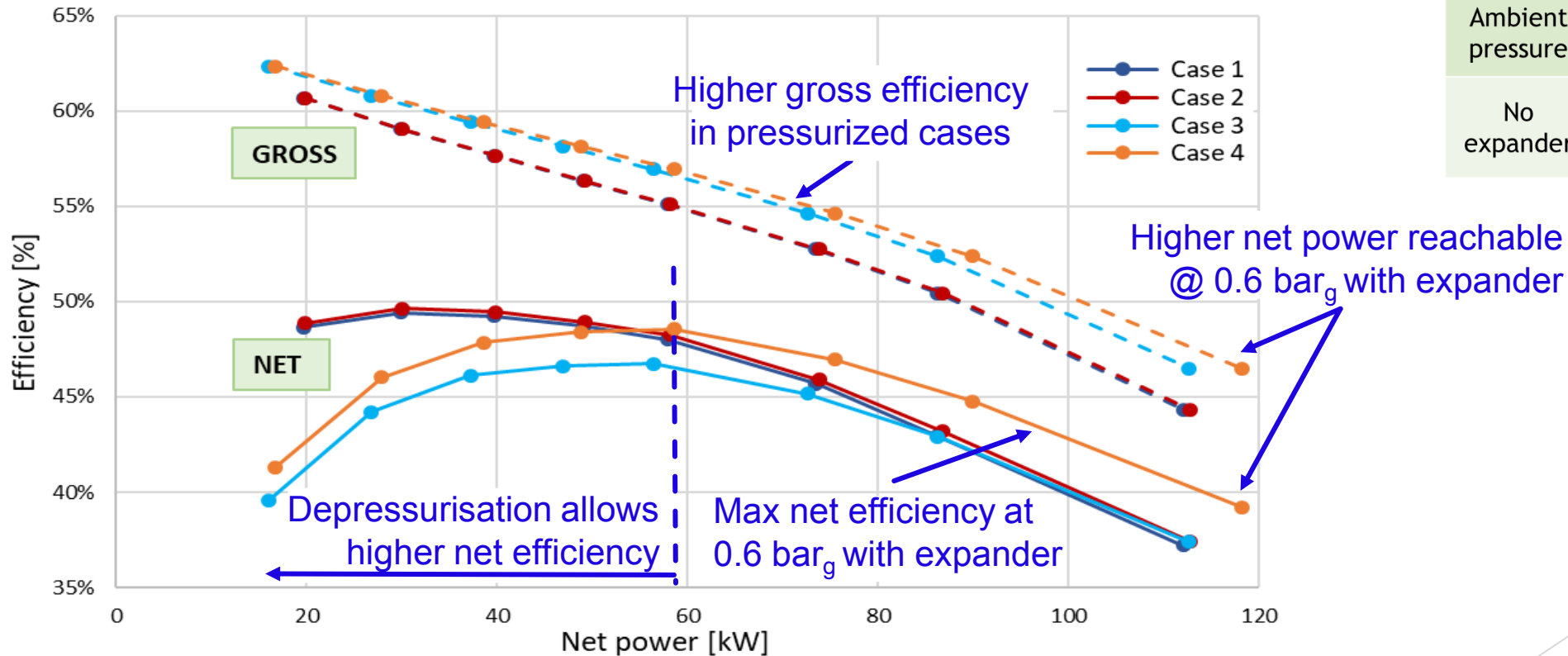
- ▶ Constant air and fuel ratio to stoichiometry.
- ▶ Variable coolant flow rate.



# Simulations results



*Gross & net efficiency*



Case 1	Case 2	Case 3	Case 4
Ambient pressure	Ambient pressure	Pressurised (0.6 bar <sub>g</sub> )	Pressurised (0.6 bar <sub>g</sub> )
No expander	With expander	No expander	With expander

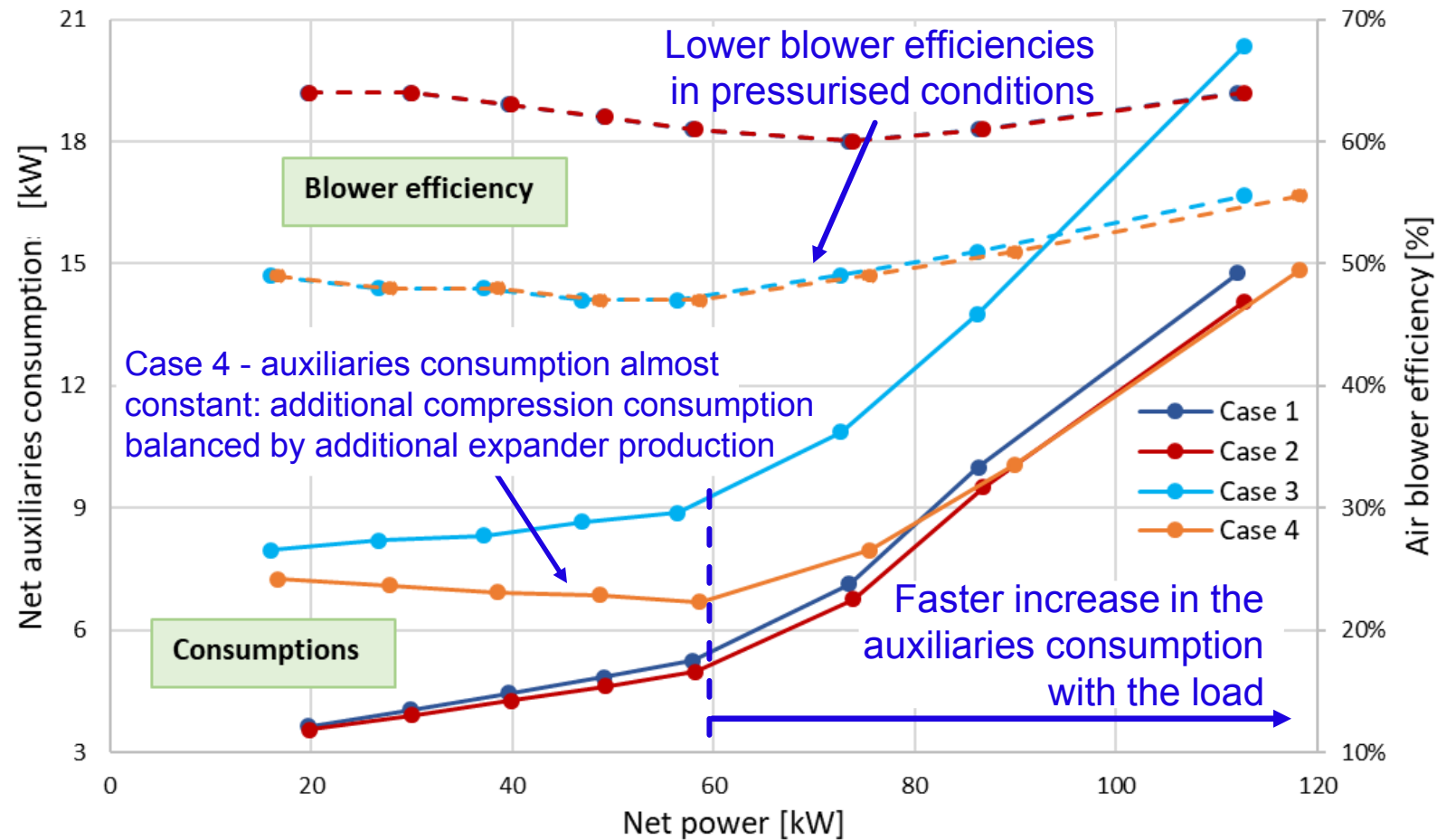
$$\eta_{GROSS} = \frac{P_{FC}}{m_{H_2} \cdot LHV}$$

$$\eta_{NET} = \frac{P_{FC} \cdot \eta_{inverter} - P_{auxiliaries}}{m_{H_2} \cdot LHV}$$

# Simulations results



*Total auxiliaries consumption and air blower efficiency*

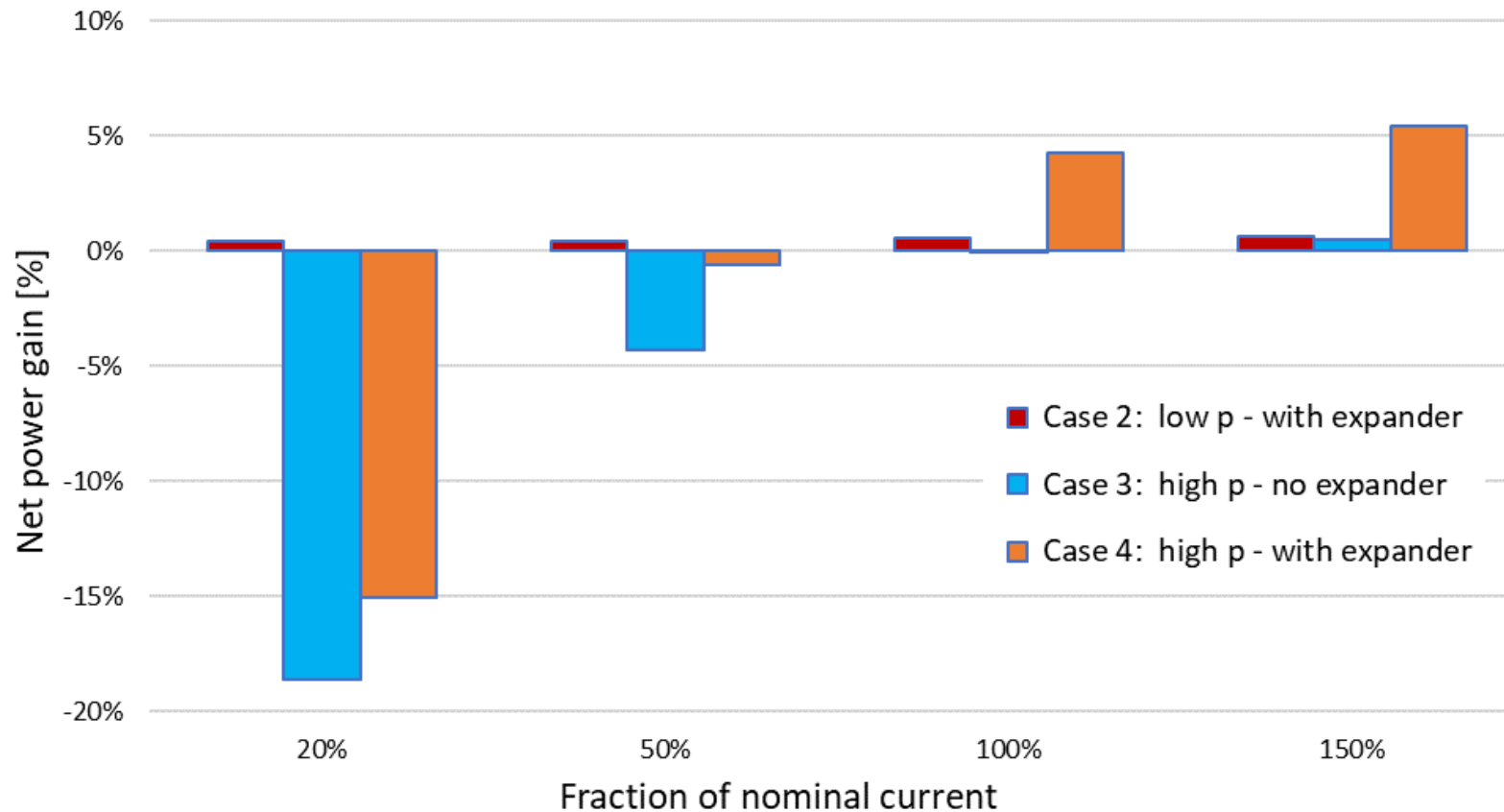


Case 1	Case 2	Case 3	Case 4
Ambient pressure	Ambient pressure	Pressurised (0.6 bar <sub>g</sub> )	Pressurised (0.6 bar <sub>g</sub> )
No expander	With expander	No expander	With expander



# Simulations results

*Net efficiency gain with respect to Case 1*

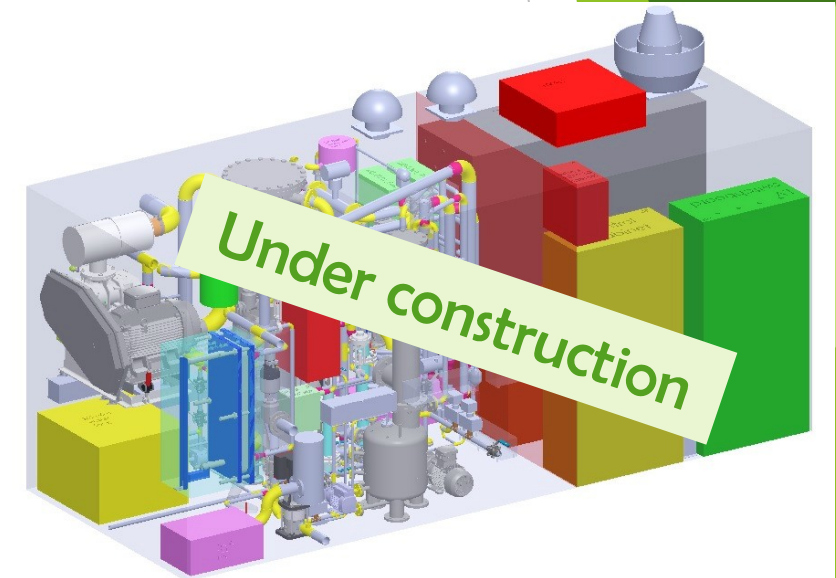


Case 1	Case 2	Case 3	Case 4
Ambient pressure	Ambient pressure	Pressurised (0.6 bar <sub>g</sub> )	Pressurised (0.6 bar <sub>g</sub> )
No expander	With expander	No expander	With expander

# Conclusions and future work



- ▶ The stationary model of the PEM FCPP has been realized and has allowed to:
  - ▶ support the decision of Grasshopper 100 kW pilot plant configuration
  - ▶ identify the operating condition maximising the plant performances at different load
  - ▶ support the definition of an optimized plant control strategy.
- ▶ Future work will consider:
  - ▶ development of new stacks and MEAs with improved performances
  - ▶ substitution of the blower with a more efficiency radial compressor to decrease the electrical losses
  - ▶ set up of a dynamic model of the pilot plant to further help in the optimization of the operation strategy.



# THANK YOU



**ABENGOA**



# Nominal operating conditions



Stack nominal operating conditions	
Nominal current density	1 A/cm <sup>2</sup>
Air ratio to stoichiometry	2
Hydrogen ratio to stoichiometry	1.5
Air / H <sub>2</sub> average RH over the stack	100 %
Stack backpressure	0.1 bar <sub>g</sub>
Stack temperature	70 °C
Coolant temperature gain over the stack	10 °C